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PATENT APPLICATION

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UNITED STATES PATENT APPLICATION

For

Monofilament Suture and Manufacturing Method Thereof

TO THE COMMISSIONER OF PATENTS AND TRADEMARKS:

Your petitioners, **Jung-nam Im, Jang-il Seo, Chong-taek Hong, Chaul-min Pai,** and **Hye-sung Yoon**, citizens of Korea, whose post office and residence addresses are Sangroksu APT 102-606, Mannyeon-dong, Seo-gu, Dae-jeon, Korea; Songgang APT 205-1010, Songgang-dong, Yuseong-gu, Dae-jeon, Korea; Cheonggu-narae APT 101-402, Jeonmin-dong, Yuseong-gu, Dae-jeon, Korea; Hanvit APT 110-402, Eoeun-dong, Yuseong-gu, Dae-jeon, Korea; and LG company house 9-301, Doryong-dong, Yuseong-gu, Dae-jeon, Korea, respectively, pray that letters patent be granted to them as the inventors of **Monofilament Suture and Manufacturing Method Thereof** as set forth in the following specification.

Monofilament Suture and Manufacturing Method Thereof

This application is a continuation-in-part of US patent application SN 10/218,336 filed on August 13, 2002, which claims benefit of Korean Patent Application No. 2002-17609
5 filed on March 30, 2002.

FIELD OF THE INVENTION

This invention relates to a monofilament suture having excellent knot security and flexibility, and to a process for the manufacture of the same.

BACKGROUND OF THE INVENTION

10 Monofilament sutures generally exhibit less tissue drag and cause less tear because they have smoother surfaces than braided multifilament sutures. Monofilament sutures, in general, do not provide the capillarity found in multifilament sutures, which minimizes the spread of wound infection with bacteria and the like. However, since monofilament sutures
15 comprise a single filament, there are the following disadvantages: they are less flexible than multifilament sutures; it is more difficult to tie a knot; and the tied knot is more likely to loosen due to inferior knot security.

Particularly, monofilament sutures are less flexible, which results in difficulties in handling and in tying during surgical operations. Moreover, due to the fact that the ears of
20 the tied suture remaining inside the body may irritate adjacent tissues, patients often complain of pain. In addition, even if a marketed monofilament suture is relatively flexible, its knot is easily untied. Therefore, in order to make the knot secure, additional throws while tying are required. Such additional throws increase the amount of suture remaining inside the body, and, consequently, increase the irritation caused by the foreign material in the wound. This
25 increase in foreign body, even in the case of an absorbable suture with good biocompatibility, may provoke irritation in adjacent tissues, and thus, increase the probability of inflammation. Furthermore, a patient may feel sensations or stimulation from the knots. The larger the volume of tied knots there is, the more likely it is that undesirable symptoms will present. Van Rijssel EJC, et al., Mechanical performance of square knots and sliding knots in surgery:
30 A comparative study, *Am J Obstet Gynecol* 1990; 162:93-7, Van Rijssel EJC, et al.; Tissue reaction and surgical knots: the effect of suture size, knot configuration, and knot volume, *Obstet Gynecol* 1989; 74:64-8; and Trimbos, J. B., Security of various knots commonly used in surgical practice, *Obstet Gynecol.*, 64:274-80, 1984.

In order to overcome the above disadvantages of a monofilament suture, various methods for improving the flexibility of monofilaments have been developed. For example, there is disclosed a process for manufacturing monofilament sutures by modification of a homopolymer (USP 5,451,461) or by using a copolymer (Monocryl[®] suture, a new ultra-pliable absorbable monofilament suture, *Biomaterials*, v16, 1995, pp 1141-1148). However, the process has limits in improving the flexibility of the suture. Also, even when flexibility is improved, the problem of poor knot security remains. When two or more polymers are combined together, disadvantages of one polymer may be offset by advantages of the others.

USP 5,626,611; 5,641,501; 6,090,910; and 6,162,537 disclose processes for preparing a suture by using different polymers. They also disclose techniques for controlling the absorption rate when absorbable sutures are degraded in the body. USP 5,641,501 and USP 6,090,910 relate to sutures prepared by physically mixing two kinds of polymers. When two polymers are physically mixed and spun into a yarn, the two polymers are not homogeneously distributed over each other, and phases of melted polymers are easily separated therefrom. Thus, it is hard to spin the polymers into yarn and it is difficult to fabricate sutures having homogeneous physical properties.

USP 5,626,611 relates to a suture prepared by co-extruding polymers into a sheath/core type, in order to control the absorption rate of the suture. That is, it relates to a method for controlling the absorption rate in accordance with the absorption rate of each polymer used in the sheath or core portion. USP 6,162,537 relates to a process for co-extruding a non-absorbable polymer and an absorbable polymer, in order to improve the biologic response of non-absorbable polymers in the body.

As described above, there has been much research in improving the flexibility and strength of sutures and into the techniques for controlling their absorption rates. However, research into improving knot security, as one of the important requirements of a suture, has not been enough. Therefore, the present invention provides a suture with excellent knot security and flexibility, which helps overcome the disadvantages of currently marketed monofilament sutures.

SUMMARY OF THE INVENTION

The present invention provides a monofilament suture that exhibits excellent knot security, flexibility and/or knot strength.

The present invention also provides a process for manufacturing a suture by a co-extrusion method that can improve spinnability.

The present invention relates to a monofilament suture prepared by co-extruding polymers with different Young's moduli and to a process for preparing the same. The suture of the present invention has excellent knot security and flexibility. The term "Young's modulus" in the present invention means a value obtained by measuring the tensile strength of yarns prepared by spinning the polymers under suitable conditions and drawing them at a draw ratio of 3~12.

The monofilament suture of the present invention is prepared by co-extruding a polymer having a high Young's modulus (first polymer) and other polymers having a low Young's modulus (second polymer) into a form so that the first polymer surrounds the second polymer. One type of suture suitable for the present invention is a sea/island type wherein the first polymer, having a high Young's modulus, is a sea component and the second polymer, having a low Young's modulus, is an island component. Another suitable type of suture of the present invention is a sheath/core type prepared from the first polymer, having a high Young's modulus, as a sheath component and the second polymer, having a low Young's modulus, as a core component.

The kinds of polymers used in the present invention are not limited, as long as they have a form so that the first polymer, with a high Young's modulus, surrounds the second polymer, with a low Young's modulus. The first polymer, or the second polymer, may be a homopolymer or a copolymer and preferably is bioabsorbable. Preferably, the first or the second polymer is a homopolymer prepared from the group consisting of glycolide, glycolic acid, lactide, lactic acid, caprolactone, dioxanone, trimethylene carbonate, ethylene glycol, derivatives thereof and copolymers thereof. For example, polycaprolactone and a copolymer thereof, polydioxanone and a copolymer thereof, a copolymer of polylactide, a copolymer of polyglycolic acid, a copolymer of trimethylene carbonate and the like may be used as the second polymer.

Preferably, the first polymer is a polyglycolic acid, polydioxanone, a polylactide or a copolymer thereof, and the second polymer is polycaprolactone, trimethylene carbonate, a homopolymer of DL-polylactide or a copolymer thereof. Alternatively, a copolymer comprising dioxanone, trimethylene carbonate and caprolactone may be employed as the second polymer. Preferably, the content of the dioxanone is within the range of 70 to 98 mole%, and the content of the trimethylene carbonate is within the range of 1 to 15 mole%, and the content of the caprolactone is within the range of 1 to 15 mole%.

If the second polymer is a copolymer, it is preferred that one or more of the same monomer is used in the first and second polymer. For example, the first polymer is

homopolymer or copolymer of polydioxanone, the second polymer is copolymer prepared from dioxanone such as a copolymer consisting of dioxanone, trimethylene carbonate and caprolactone may be employed as the second polymer.

In the present invention, a given polymer may be used as the first polymer or the second polymer. That is, even though the same polymer is used, the position of the polymer depends on the Young's modulus of the other polymer used during their co-extrusion. Specifically, when a sea/island type suture is prepared by using polydioxanone and polycaprolactone, polydioxanone is used as the sea component (the first polymer) and polycaprolactone as the island component (the second polymer), since the Young's modulus of polydioxanone is higher than that of polycaprolactone. However, when polydioxanone and polyglycolic acid are co-extruded into a sea/island type, polydioxanone must be used as the island component (the second polymer) and polyglycolic acid as the sea component (the first polymer), since the Young's modulus of polydioxanone is lower than that of polyglycolic acid.

In the present invention, co-extrusion of the polymers into the sea/island type is more desirable than co-extrusion of the polymers into the sheath/core type. Even though the content ratios of the two polymers used are the same, the cross-sectional shape of the suture prepared as the sea/island type is greatly deformed by tying the knot, and thus, surface friction force is increased even more. Therefore, the suture made by co-extrusion of the polymers into the sea/island type of the present invention gives excellent knot security.

Generally, fibers become more flexible when their stiffness is low. Stiffness varies with the cross sectional shape of the fibers, even when they have the same cross-sectional area. The sea/island type suture is more flexible than the sheath/core type suture, due to the cross-sectional shape of the second polymer. It is generally believed that stiffness of the sea/island type suture is low. However, among sea/island type sutures with the same component ratios, the physical properties of the suture may vary depending on the number of islands or the arrangement of the islands.

Preferably, in the present invention, the first polymer, having a higher Young's modulus, also has a higher melting point than the second polymer. When co-extruding the first polymer, whose Young's modulus and melting point are lower than the second polymer, the resulting suture is not round in cross-section (Ref. FIG. 4b), and has poor knot strength. Therefore, it would not be suitable for use as a suture. If the cross-sectional roundness of a suture deteriorates, the suture is apt to cause tissue dragging and difficulties in needle attachment, and therefore, would not be suitable for use as a suturing material.

In the present invention, the amount of the first polymer is preferably 10 –90% by volume, and the amount of the second polymer is preferably 10 – 90% by volume. When the amount of each polymer is less than 10% by volume, a cross section of the obtained suture does not clearly distinguish between the first polymer and the second polymer. Thus, it is preferred that each polymer is used in an amount of 10% by volume or more. More preferably, the amount of the first polymer is 50 – 90% by volume and the amount of the second polymer is 10 – 50% by volume. When the amount of the second polymer is 50% or more, the surface layer of first polymer becomes too thin. Therefore, there is an operational problem in that the second polymer is drawn near the surface of the suture and the resulting yarn is more likely to break during the manufacturing process. In addition, when an annealing process is carried out, for improving the mechanical properties of the suture, the second polymer, the amount of which is too large, is likely to be exposed outward from the first polymer, and thus, the surface of the suture is apt to be rough. When the surface becomes rough, the suture will likely cause damage such as tissue dragging.

Preferably, the first polymer and the second polymer used in the present invention are polymers that have a Young's modulus of 3.0GPa or less. When the Young's modulus is more than 3.0GPa, the obtained suture is not suitable for use as a monofilament suture, since its flexibility is low, even though the polymers are co-extruded. More preferably, the first polymer has a Young's modulus of 2.0GPa or less. If the Young's modulus of the first polymer is high, it will easily cause shape deformation of the monofilament and cause surface unevenness and/or cracking of the knot when it is tied, which in turn provides the advantage of improving knot security. However, when the Young's modulus of the first polymer is too high, i.e. 2.0GPa or more, the flexibility of the monofilament is lowered even when the monofilaments are prepared by co-extrusion.

In the present invention, the second polymer preferably has a Young's modulus of 1.5 GPa or less, and more preferably, the second polymer has a Young's modulus of 1.2 GPa or less. The sutures become more flexible when the Young's moduli of the polymers are lower.

More preferably, a polymer having Young's modulus of 1.0~1.5 GPa is used as the first polymer with the second polymer having a Young's modulus of at least 0.3 GPa lower than the Young's modulus of the first polymer.

The surface unevenness, by knot tying, is larger when the difference of the Young's moduli between the first polymer and the second polymer is larger. Therefore, it is preferred that the second polymer of the present invention has a Young's modulus of 0.4~1.2 GPa.

The suture obtained by the present invention has excellent knot security and flexibility. Therefore, it may be used in soft tissue patches, surgical mesh, thin film type dressings, surgical felts, artificial blood vessels, auxiliary materials for treating nerves, artificial skins, sternum tapes, sutures and the like.

5 In addition to promoting wound repair and/or tissue growth, a small amount of a drug may be added to the first or second polymer. Also, for improving knot security and flexibility, a small amount of various polymers and/or additives may be added to one of the above polymers. Therefore, the purpose of the present invention also includes co-extruding these polymers with the first and the second polymer of the present invention.

BRIEF DESCRIPTION OF DRAWINGS

FIGs. 1a and 1b are schematic prespective views of the final filament shape to be realized by the present invention (1a: sea/island type, 1b: sheath/core type).

15 FIG. 2 illustrates schematically a process for manufacturing the suture to be obtained in the present invention.

FIGs. 3a and 3b illustrate schematically a spinning pack (nozzle pack) (3a: the spinning pack for preparing the sea/island type suture, 3b: the spinning pack for preparing the sheath/core type suture).

20 FIG. 4a is an SEM photograph showing a cross section of the suture obtained by co-extruding a polymer with a high Young's modulus surrounding a polymer with a low Young's modulus.

FIG. 4b is an SEM photograph showing a cross section of the suture obtained by co-extruding a polymer with a low Young's modulus surrounding a polymer with a high Young's modulus.

25 FIGs. 5a and 5b are SEM photographs showing cross sections of knots tied with the sutures obtained by the present invention.

FIG. 6a represents the knot configuration of the suture obtained by co-extruding polydioxanone and polycaprolactone into the sea/island type suture.

30 FIG. 6b represents the knot configuration of the suture obtained by co-extruding polylactide and polycaprolactone.

FIG. 6c is an SEM photograph showing the knot configuration of the suture prepared from polydioxanone only.

FIGs. 7a-7c illustrate DIC photographs showing that the cross section varies with the component ratios of the monofilament suture prepared in accordance with the present invention (by the content ratio of the sea component, 7a: 70%, 7b: 50%, 7c: 20%).

DETAILED DESCRIPTION THE INVENTION

This invention is not limited to the particular configurations, process steps, and materials disclosed herein, as such configurations, process steps, and materials may vary somewhat. It is also to be understood that the terminology employed herein is used for the purpose of describing particular embodiments only, and is not intended to be limiting since the scope of the present invention will be limited only by the appended claims and equivalents thereof.

In this specification and the appended claims, the singular forms "a," "an," and "the" include plural references unless the context clearly dictates otherwise. In describing and claiming the present invention, the following terminology will be used in accordance with the definitions set out below.

"Biodegradable polymer" and "absorbable polymer" means that the polymer can chemically break down or degrade within the body to form nontoxic components.

The present invention relates to preparing monofilament sutures by co-extrusion of two biodegradable polymers having different Young's Moduli, which is explained in view of the attached figures as follows:

FIGs. 1a and 1b illustrate the final shapes of the filaments to be embodied by the present invention. A monofilament 10 is co-extruded in the sea/island type, wherein the island component 11 is surrounded by the sea component 12. A monofilament 13 is co-extruded in the sheath/core type, wherein the core component 14 is surrounded by the sheath component 15. Since the components making up the filaments and their sutures affect the physical properties, the characteristics of each filament 10, 13 are different from those of conventional coated filaments.

FIG. 2 schematically illustrates the conventional manufacturing process used to produce co-extruded monofilaments having the structure of the present invention.

Specifically, in the co-extrusion process, each polymer is separately melted by two extruders 21. The melted polymers flow out in the desired amounts through the metering pumps 22. By controlling the amounts that flow, the content ratio of each polymer can be controlled in the co-extruded polymers.

The melted polymers, which flowed out through metering pump 22, are combined in the manner shown in FIGs 3a and 3b, into filament 24 through spin block 23. Although a single filament is shown for simplification in FIG 2, it is understood that spinnerets having any desired number of exiting orifices may be used. The melted filament 24 is solidified in quenching bath 25. The air gap is the distance between the spinneret exit and the bath. Preferably the air gap distance ranges from 0.5 to 100 centimeters and, more preferably, from about 1 to 30 centimeters. The solidified yarn 24 is drawn with drawing system 26 in order to achieve the desired orientation and improve the physical properties. After that, the finished monofilament product is wound to winder 27. Alternatively, in order to improve the physical properties of the suture, the solidified yarn 24 is not directly drawn, but is wound in the form of undrawn yarn (UDY). It may be aged under appropriate conditions, and then, drawn by a drawing system to prepare the drawn yarn. Following the drawing process, the monofilament 24 may be annealed to further improve its properties.

FIGs. 3a and 3b illustrate examples of a spin pack which may be used as a spin block 23 in the present invention and which comprises a nozzle, distribution plates and the like. The first polymer and the second polymer are melted through each extruder, passed through distribution plates 31 and 36, and each flow into a nozzle 32, where the melted polymers are joined thus forming a continuous polymer melt.

Specifically, FIG. 3a is an example of the spin pack for obtaining a sea/island type suture. The first polymer and the second polymer pass through distribution plates 31. The second polymer, passing through flow channels 33, becomes the island component, and the first polymer, passing through flow channels 34, becomes the sea component surrounding the second polymer.

The number of flow channels 33 varies with the desired physical properties of the final filament. If the number of flow channels is one, the polymers become a co-extruded sheath/core type filament as shown in FIG. 3b. FIG. 3b is an example of the spin pack for preparing a sheath/core type suture. The melted second polymer, used to form the core component, passes through the center flow channel 37, and the melted first polymer passing through outer flow channel is incorporated into a single filament at the nozzle 32.

In the suture obtained by the above process, knot security, flexibility and strength of the suture may be controlled by using polymers having Young's moduli, strengths and melting points which are different from each other and controlling the content ratio of each polymer.

The present invention improves the knot security and flexibility of a suture by co-extruding polymers having different Young's moduli to prepare a monofilament suture in a form so that a polymer with a high Young's modulus surrounds a polymer with a low Young's modulus. The suture obtained by the present invention may be used as a medical
5 appliance such as an artificial tendon, soft tissue patch, surgical mesh, thin film type dressing, surgical felt, artificial blood vessel, artificial skin, sternum tape and the like as well as be used as a suture.

The present invention, hereinafter, is explained in more detail, based on the following examples and comparative examples. However, these examples are provided for
10 the purpose of illustrating the present invention only, and thus, the present invention is not intended to be limited to the examples in any way.

Methods for measuring the physical properties of sutures – knot security

Knot security was measured in terms of the knot slippage ratio. A surgeon's knot (2=1=1) was selected for the knot tying method. The knotted sutures were placed on a tensile
15 strength tester and pulled apart until knot breakage occurred or the knot slipped. After ten measurements, the ratio of the number of knots slipped to the total number of the knots tied indicates the knot slippage ratio. Thus, the less the ratio is, the better the knot security of the suture.

Methods for measuring the physical properties of sutures – flexibility

Most reported flexibility data of sutures are based on Young's moduli derived from
20 measuring linear tensile strength. However, the flexibility derived from the Young's modulus may be misleading in evaluating suture material because it represents flexibility in the tensile mode, which may be quite different from the bending stiffness that a suture actually experiences during wound closure. Therefore, in the present invention, bending
25 stiffness was measured as a barometer of flexibility. The less the value, the more flexible the suture is.

Methods for measuring the physical properties of the suture are set forth in Table 1.

Table 1

Methods for measuring the physical properties of the suture

Physical Property	Method for Measuring and Apparatus
Diameter, mm	EP regulation, Diameter
Knot strength, kgf	EP regulation, Tensile Strength Instron Corporation
Stiffness, mgf/mm ²	Stiffness Gurley Stiffness Tester
Knot slippage ratio, %	Surgeon's Knot (2=1=1) Instron Corporation

Example 1

In this example, polydioxanone having a relative viscosity of 2.3 dl/g (measured with HFIP solution of 0.1 g/dl at 25 °C) was used as the first polymer and polycaprolactone having a relative viscosity of 1.7 dl/g (measured with a chloroform solution of 0.2 g/dl at 25 °C) as the second polymer. A sea/island type monofilament suture was prepared in accordance with the parameters, terms and conditions as set forth in Table 2 below. By the method for measuring the physical properties explained above, diameter, knot strength, stiffness and knot slippage ratio of the prepared suture were measured.

Table 2

Conditions of Processing the Sea/Island Type Co-extruded Suture

Suture Size		EP 4	
Polymer		Polycaprolactone	Polydioxanone
Young's modulus (GPa)		0.7	1.3
Melting Point (°C)		55~65	95~110
Process Conditions		Extrusion Conditions	
Extruder		Ext. 1 (Island)	Ext. 2 (Sea)
Number of Island Component		19	-
Extruder screw, rpm		7.5	11.4
Manifold* pressure (kgf/cm ²)		80	80
Temperature of Extruder (°C)	Zone 1	175	180
	Zone 2	178	183
	Zone 3	180	185
Temperature of Manifold (°C)		180	185
Temperature of Metering pump (°C)		180	185
Temperature of Nozzle Pack Die (°C)		185	
Capacity of Metering pump (cc/rev)		1.2	1.2

Revolution of Metering pump (rpm)	4.0	9.3
Temperature of Quenching bath (°C)	23	
Winding Speed of Undrawn yarn (m/min)	13.4	
	Drawing Conditions	
First Roller (m/min)	4.4	
Temperature of First Drawing Oven (°C)	110	
Second Roller (m/min)	26.6	
Temperature of Second Drawing Oven (°C)	115	
Third Roller (m/min)	27.3	
Temperature of Third Drawing Oven (°C)	115	
Fourth Roller (m/min)	22.0	
Total Drawing Ratio	5.0	

*Manifold – Connecting site between extruder and metering pump

Example 2

- In this example, a copolymer of glycolic acid and caprolactone in a ratio of 75/25 having a relative viscosity of 1.4 dl/g (measured with a HFIP solution of 0.5 g/dl at 25 °C) was used as the first polymer and polycaprolactone having a relative viscosity of 1.5 dl/g (measured with a chloroform solution of 0.2 g/dl at 25 °C) was used as the second polymer. A sea/island type monofilament suture was prepared in accordance with the parameters, terms and conditions as set forth in Table 3 below. Using the method for measuring the physical properties explained above, diameter, knot strength, stiffness and knot slippage ratio of the prepared suture were measured.

Table 3

Conditions of Processing the Sea/Island Type Co-extruded Suture

Suture Size		EP 4	
Polymer		Polycaprolactone	Copolymer*
Young's modulus (GPa)		0.7	1.1
Melting Point (°C)		55-65	210-220
Process Conditions		Extrusion Conditions	
Extruder		Ext. 1 (Island)	Ext. 2 (Sea)
Number of Island Component		19	-
Extruder screw, rpm		7.6	22.3
Manifold pressure (kgf/cm ²)		80	80
Temperature of Extruder (°C)	Zone 1	170	210
	Zone 2	180	215
	Zone 3	190	220
Temperature of Manifold (°C)		190	230
Temperature of Metering pump (°C)		190	230
Temperature of Nozzle Pack Die (°C)		240	
Capacity of Metering pump (cc/rev)		1.2	1.2

Revolution of Metering pump (rpm)	8.0	12.0
Temperature of Quenching bath (°C)	5	
Winding Speed of Undrawn yarn (m/min)	18.1	
	Drawing Conditions	
First Roller (m/min)	4.4	
Temperature of First Drawing Oven (°C)	90	
Second Roller (m/min)	26.0	
Temperature of Second Drawing Oven (°C)	120	
Third Roller (m/min)	29.3	
Temperature of Third Drawing Oven (°C)	120	
Fourth Roller (m/min)	26.4	
Total Drawing Ratio	6.0	

* Copolymer of glycolic acid and caprolactone

Example 3

In this example, polydioxanone having a relative viscosity of 2.3 dl/g (measured with a HFIP solution of 0.1 g/dl at 25 °C) was used as the first polymer and a copolymer of lactide and caprolactone in a ratio of 90/10 having a molecular weight (Mw) of about 200,000 (measured by GPC) was used as the second polymer. A sea/island type monofilament suture was prepared in accordance with the parameters, term and conditions as set forth in Table 4 below. Using the method for measuring the physical properties explained above, diameter, knot strength, stiffness and knot slippage ratio of the prepared suture were measured.

Table 4

Conditions of Processing the Sea/Island Type Co-extruded Suture

Suture Size		EP 3	
Polymer		Copolymer*	Polydioxanone
Young's modulus (GPa)		0.6	1.3
Melting Point (°C)		Amorphous	95~110
Process Conditions		Extrusion Conditions	
Extruder		Ext. 1 (Island)	Ext. 2 (Sea)
Number of Island Component		37	-
Extruder screw, rpm		7.3	11.5
Manifold pressure (kgf/cm ²)		80	80
Temperature of Extruder (°C)	Zone 1	140	180
	Zone 2	145	183
	Zone 3	150	185
Temperature of Manifold (°C)		150	185
Temperature of Metering pump (°C)		150	185
Temperature of Nozzle Pack Die (°C)		185	
Capacity of Metering pump (cc/rev)		1.2	1.2
Revolution of Metering pump (rpm)		4.0	9.3

Temperature of Quenching bath (°C)	2
Winding Speed of Undrawn yarn (m/min)	31.1
	Drawing Conditions
First Roller (m/min)	5.3
Temperature of First Drawing Oven (°C)	100
Second Roller (m/min)	26.6
Temperature of Second Drawing Oven (°C)	105
Third Roller (m/min)	27.7
Temperature of Third Drawing Oven (°C)	105
Fourth Roller (m/min)	25.0
Total Drawing Ratio	4.7

* Copolymer of lactide and caprolactone

Example 4

In this example, polydioxanone having a relative viscosity of 2.6 dl/g (measured with a HFIP solution of 0.1 g/dl at 25 °C) was used as the first polymer and a block terpolymer consisting of dioxanone (90mole%), trimethylene carbonate (9mole%) and caprolactone (1mole%) and having a relative viscosity of 2.2 dl/g (measured with an HFIP solution of 0.1 g/dl at 25 °C) were used as the second polymer. A sea/island type monofilament suture was prepared in accordance with the parameters, term and conditions as set forth in Table 5 below. Using the method for measuring the physical properties explained above, diameter, knot strength, stiffness and knot slippage ratio of the prepared suture were measured.

Table 5

Conditions of Processing the Sea/Island Type Co-extruded Suture

Suture Size		EP 4	
Polymer		Copolymer*	Polydioxanone
Young's modulus (GPa)		0.85	1.3
Melting Point (°C)		95~110	95~110
Process Conditions		Extrusion Conditions	
Extruder		Ext. 1 (Island)	Ext. 2 (Sea)
Number of Island Component		8	-
Extruder screw, rpm		9.4	4.5
Manifold pressure (kgf/cm ²)		80	80
Temperature of Extruder (°C)	Zone 1	175	170
	Zone 2	180	172
	Zone 3	180	175
Temperature of Manifold (°C)		180	175
Temperature of Metering pump (°C)		180	175
Temperature of Nozzle Pack Die (°C)		175	
Capacity of Metering pump (cc/rev)		1.168	1.2
Revolution of Metering pump (rpm)		7.0	3.0

Temperature of Quenching bath (°C)	24
Winding Speed of Undrawn yarn (m/min)	9.8
Drawing Conditions	
First Roller (m/min)	6.0
Temperature of First Drawing Oven (°C)	90
Second Roller (m/min)	29.5
Temperature of Second Drawing Oven (°C)	95
Third Roller (m/min)	31.2
Temperature of Third Drawing Oven (°C)	95
Fourth Roller (m/min)	25.0
Total Drawing Ratio	4.2

*Block terpolymer consisting of dioxanone, trimethylene carbonate and caprolactone

Example 5

- In this example, polydioxanone having a relative viscosity of 2.6 dl/g (measured with HFIP solution of 0.1 g/dl at 25°C) was used as the first polymer and a block terpolymer consisting of dioxanone (83mole%), trimethylene carbonate (13mole%) and caprolactone (4mole%) and having a relative viscosity of 2.1 dl/g (measured with HFIP solution of 0.1 g/dl at 25°C) were used as the second polymer. A sea/island type monofilament suture was prepared in accordance with the parameters, term and conditions as set forth in Table 6 below. Using the method for measuring the physical properties explained above, diameter, knot strength, stiffness and knot slippage ratio of the prepared suture were measured.

Table 6

Conditions of Processing the Sea/Island Type Co-extruded Suture

Suture Size		EP 2	
Polymer		Copolymer*	Polydioxanone
Young's modulus (GPa)		0.85	1.3
Melting Point (°C)		95~110	95~110
Process Conditions		Extrusion Conditions	
Extruder		Ext. 1 (Island)	Ext. 2 (Sea)
Number of Island Component		8	-
Extruder screw, rpm		5.6	3.0
Manifold pressure (kgf/cm ²)		80	80
Temperature of Extruder (°C)	Zone 1	175	170
	Zone 2	178	172
	Zone 3	180	175
Temperature of Manifold (°C)		180	175
Temperature of Metering pump (°C)		180	175
Temperature of Nozzle Pack Die (°C)		175	
Capacity of Metering pump (cc/rev)		1.168	1.2

Revolution of Metering pump (rpm)	4.9	2.1
Temperature of Quenching bath (°C)	21	
Winding Speed of Undrawn yarn (m/min)	24.0	
	Drawing Conditions	
First Roller (m/min)	6.0	
Temperature of First Drawing Oven (°C)	90	
Second Roller (m/min)	29.5	
Temperature of Second Drawing Oven (°C)	95	
Third Roller (m/min)	31.2	
Temperature of Third Drawing Oven (°C)	95	
Fourth Roller (m/min)	22.2	
Total Drawing Ratio	3.7	

*Block terpolymer consisting of dioxanone, trimethylene carbonate and caprolactone

Example 6

In this example, polydioxanone having a relative viscosity of 2.4 dl/g (measured with an HFIP solution of 0.1 g/dl at 25 °C) was used as the first polymer and polycaprolactone having a relative viscosity of 1.7 dl/g (measured with a chloroform solution of 0.2 g/dl at 25 °C) as the second polymer. A sheath/core type monofilament suture was prepared in accordance with the parameters, terms and conditions as set forth in Table 7 below. Using the method for measuring the physical properties explained above, diameter, knot strength, stiffness and knot slippage ratio of the prepared suture were measured:

Table 7

Conditions of Processing the Sheath/Core Type Co-extruded Suture

Suture Size		EP 4	
Polymer		Polycaprolactone	Polydioxanone
Young's modulus (GPa)		0.7	1.3
Melting Point (°C)		55~65	95~110
Process Conditions		Extrusion Conditions	
Extruder		Ext. 1 (Core)	Ext. 2 (Sheath)
Extruder screw, rpm		6.8	11.8
Manifold pressure (kgf/cm ²)		80	80
Temperature of Extruder (°C)	Zone 1	175	180
	Zone 2	178	183
	Zone 3	180	185
Temperature of Manifold (°C)		180	185
Temperature of Metering pump (°C)		180	185
Temperature of Nozzle Pack Die (°C)		185	
Capacity of Metering pump (cc/rev)		1.2	1.2
Revolution of Metering pump (rpm)		4.0	9.3
Temperature of Quenching bath (°C)		21	

Winding Speed of Undrawn yarn (m/min)	13.7
	Drawing Conditions
First Roller (m/min)	4.4
Temperature of First Drawing Oven (°C)	110
Second Roller (m/min)	26.6
Temperature of Second Drawing Oven (°C)	115
Third Roller (m/min)	27.3
Temperature of Third Drawing Oven (°C)	115
Fourth Roller (m/min)	22.0
Total Drawing Ratio	5.0

Comparative Example 1

In this example, polycaprolactone having a relative viscosity of 1.7 dl/g (measured with a chloroform solution of 0.2 g/dl at 25 °C) was used as the sea component and polydioxanone having a relative viscosity of 2.3 dl/g (measured with a chloroform solution of 0.1 g/dl at 25 °C) as the island component. A sea/island type monofilament suture was prepared in accordance with the parameters, terms and conditions as set forth in Table 8 below. Using the method for measuring the physical properties explained above, diameter, knot strength, stiffness and knot slippage ratio of the prepared suture were measured.

Table 8

Conditions of Processing the Sea/Island Type Co-extruded Suture

Suture Size		EP 4	
Polymer		Polydioxanone	Polycaprolactone
Young's modulus (GPa)		1.3	0.7
Melting Point (°C)		95~110	55~65
Process Conditions		Extrusion Conditions	
Extruder		Ext. 1 (Island)	Ext. 2 (Sea)
Number of Island Component		19	-
Extruder screw, rpm		19.2	7.8
Manifold pressure (kgf/cm ²)		80	80
Temperature of Extruder (°C)	Zone 1	180	175
	Zone 2	183	178
	Zone 3	185	180
Temperature of Manifold (°C)		185	180
Temperature of Metering pump (°C)		185	180
Temperature of Nozzle Pack Die (°C)		185	
Capacity of Metering pump (cc/rev)		1.2	1.2
Revolution of Metering pump (rpm)		14.0	6.0
Temperature of Quenching bath (°C)		8	
Winding Speed of Undrawn yarn (m/min)		25.7	

	Drawing Conditions
First Roller (m/min)	6.5
Temperature of First Drawing Oven (°C)	60
Second Roller (m/min)	26.8
Temperature of Second Drawing Oven (°C)	70
Third Roller (m/min)	27.8
Temperature of Third Drawing Oven (°C)	70
Fourth Roller (m/min)	25.1
Total Drawing Ratio	3.9

Comparative Example 2

In this example, polycaprolactone having a relative viscosity of 1.7 dl/g (measured with a chloroform solution of 0.2 g/dl at 25 °C) was used as the sea component and a copolymer of glycolic acid and caprolactone in a ratio of 75/25 having a relative viscosity of 1.5 dl/g (measured with a chloroform solution of 0.5 g/dl at 25 °C) as the island component. A sea/island type monofilament suture was prepared in accordance with the parameters, terms and conditions as set forth in Table 9 below. Using the method for measuring the physical properties explained above, diameter, knot strength, stiffness and knot slippage ratio of the prepared suture were measured.

Table 9

Conditions of Processing the Sea/Island Type Co-extruded Suture

Suture Size		EP 4	
Polymer		Copolymer	Polycaprolactone
Young's modulus (GPa)		1.1	0.7
Melting Point (°C)		210~220	55~65
Process Conditions		Extrusion Conditions	
Extruder		Ext. 1 (Island)	Ext. 2 (Sea)
Number of Island Component		19	-
Extruder screw, rpm		19.5	7.8
Manifold pressure (kgf/cm ²)		80	80
Temperature of Extruder (°C)	Zone 1	210	170
	Zone 2	215	180
	Zone 3	220	190
Temperature of Manifold (°C)		230	190
Temperature of Metering pump (°C)		230	190
Temperature of Nozzle Pack Die (°C)		230	
Capacity of Metering pump (cc/rev)		1.2	1.2
Revolution of Metering pump (rpm)		16	4
Temperature of Quenching bath (°C)		5	
Winding Speed of Undrawn yarn (m/min)		22.3	

	Drawing Conditions
First Roller (m/min)	4.6
Temperature of First Drawing Oven (°C)	60
Second Roller (m/min)	22.7
Temperature of Second Drawing Oven (°C)	70
Third Roller (m/min)	23.2
Temperature of Third Drawing Oven (°C)	70
Fourth Roller (m/min)	22.0
Total Drawing Ratio	4.8

* Copolymer of glycolic acid and caprolactone

Comparative Example 3

In this example, a copolymer of lactide and caprolactone having a molecular weight (Mw) of about 200,000 (measured by GPC) was used as the sea component and polydioxanone having a relative viscosity of 2.3 dl/g (measured with a HFIP solution of 0.1 g/dl at 25 °C) as the island component. A sea/island type monofilament suture was prepared in accordance with the parameters, terms and conditions as set forth in Table 10 below. Using the method for measuring the physical properties explained above, diameter, knot strength, stiffness and knot slippage ratio of the prepared suture were measured.

Table 10

Conditions of Processing the Sea/Island Type Co-extruded Suture

Suture Size		EP 3	
Polymer		Polydioxanone	Copolymer*
Young's modulus (G Pa)		1.3	0.6
Melting Point (°C)		95~110	Amorphous
Process Conditions		Extrusion Conditions	
Extruder		Ext. 1 (Island)	Ext. 2 (Sea)
Number of Island Component		37	-
Extruder screw, rpm		11.5	7.6
Manifold pressure (kgf/cm ²)		80	80
Temperature of Extruder (°C)	Zone 1	180	140
	Zone 2	183	145
	Zone 3	185	145
Temperature of Manifold (°C)		185	145
Temperature of Metering pump (°C)		185	150
Temperature of Nozzle Pack Die (°C)		185	
Capacity of Metering pump (cc/rev)		1.2	1.2
Revolution of Metering pump (rpm)		9.3	4.0
Temperature of Quenching bath (°C)		21	
Winding Speed of Undrawn yarn (m/min)		41.3	
		Drawing Conditions	

First Roller (m/min)	7.0
Temperature of First Drawing Oven (°C)	60
Second Roller (m/min)	25.5
Temperature of Second Drawing Oven (°C)	65
Third Roller (m/min)	26.3
Temperature of Third Drawing Oven (°C)	65
Fourth Roller (m/min)	25.0
Total Drawing Ratio	3.6

* Copolymer of lactide and caprolactone

Comparative Example 4

In this example, a block terpolymer consisting of dioxanone (90mole %),
 5 trimethylene carbonate (9mole %) and caprolactone (1mole %) and having a relative
 viscosity of 2.2 dl/g (measured with HFIP solution of 0.1 g/dl at 25 °C) was used as the sea
 component and polydioxanone having a relative viscosity of 2.6 dl/g (measured with a HFIP
 solution of 0.1 g/dl at 25 °C) as the island component. A sea/island type monofilament suture
 was prepared in accordance with the parameters, terms and conditions as set forth in Table 11
 10 below. Using the method for measuring the physical properties explained above, diameter,
 knot strength, stiffness and knot slippage ratio of the prepared suture were measured.

Table 11

Conditions of Processing the Sea/Island Type Co-extruded Suture

15

Suture Size		EP 4	
Polymer		Polydioxanone	Copolymer*
Young's modulus (G Pa)		1.3	0.85
Melting Point (°C)		95~110	95~110
Process Conditions		Extrusion Conditions	
Extruder		Ext. 1 (Island)	Ext. 2 (Sea)
Number of Island Component		8	-
Extruder screw, rpm		5.1	8.9
Manifold pressure (kgf/cm ²)		80	80
Temperature of Extruder (°C)	Zone 1	170	175
	Zone 2	174	178
	Zone 3	175	180
Temperature of Manifold (°C)		175	180
Temperature of Metering pump (°C)		175	180
Temperature of Nozzle Pack Die (°C)		180	
Capacity of Metering pump (cc/rev)		1.168	1.2
Revolution of Metering pump (rpm)		3.0	7.0
Temperature of Quenching bath (°C)		24	
Winding Speed of Undrawn yarn (m/min)		9.8	

	Drawing Conditions
First Roller (m/min)	6.0
Temperature of First Drawing Oven (°C)	110
Second Roller (m/min)	29.5
Temperature of Second Drawing Oven (°C)	115
Third Roller (m/min)	31.2
Temperature of Third Drawing Oven (°C)	115
Fourth Roller (m/min)	25.0
Total Drawing Ratio	4.2

*Block teropolymer consisting of dioxanone, trimethylene carbonate and caprolactone

The physical properties of sutures prepared in accordance with the above examples are set forth in Table 12 below.

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Table 12

Physical Properties of Sutures

Measuring Items	Examples						Comparative Examples			
	1	2	3	4	5	6	1	2	3	4
Size	EP 4	EP 4	EP 3	EP3.5	EP 2	EP 4	EP 4	EP 4	EP 3	EP3.5
Diameter, mm	0.549	0.532	0.373	0.487	0.282	0.545	0.552	0.535	0.370	0.463
Knot Strength, kgf	5.5	6.0	3.3	6.21	2.1	4.9	3.1	3.5	1.8	4.19
Stiffness, mgf/mm ²	80	72	55	65	23	106	100	85	73	59
Knot slippage ratio, %	0	0	10	0	0	0	10	30	40	20

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As shown in Table 12, the physical properties of sutures prepared by using the polymer polymer with a high Young's modulus as the first polymer in accordance with the present invention have excellent knot security and flexibility. In addition, monofilament sutures with excellent knot strength can also be obtained.

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Specifically, since sutures obtained in Example 1 and Comparative Example 1 are co-extruded by using polydioxanone and polycaprolactone; both sutures have an EP 4 size and have diameters similar to each other. However, despite having similar diameters, the suture of Example 1, using polydioxanone with a high Young's modulus as the first polymer, is less stiff than the suture of Comparative Example 1. Therefore, it is shown that in the case of preparing sutures in accordance with the present invention, more flexible sutures can be obtained.

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In addition, in the case of preparing monofilament sutures in accordance with the present invention, the knot slippage ratio is 0%, meaning the tied knot does not loosen.

However, in the case of preparing the suture in a form so that the polymer with a low Young's modulus surrounds the polymer with a high Young's modulus, as in Comparative Examples 1, 2, 3 and 4, the knot security is less. Also, in the case of preparing the suture in a form so that the polymer with a low Young's modulus surrounds the polymer with a high Young's modulus, the knot strength is significantly lowered as in Comparative Example 1. In order to increase the knot strength of the suture, in the case of increasing the draw ratio, roundness is not a suitable shape to use as a suture, as shown in FIG. 4b. The reason is considered to be as follows: when drawing force is added to the polymer with a low Young's modulus being used as the surrounding polymer under the drawing process, the shape of the polymer is easily deformed.

Experimental Example 1

In order to compare the sea/island type suture with the sheath/core type suture, the sutures were prepared by extruding polydioxanone as the first polymer and polycaprolactone as the second polymer and drawing the extrudate. At this time, in the case of the sea/island type, the number of the island component was 7. The physical properties of the sutures were measured.

Table 13

Comparison of the physical properties of the sea/island type suture with the sheath/core type suture

		Knot strength (Gpa)	Stiffness (mgf/mm ²)
PDO 50%	Sea/island type	0.134	57
PCL 50%	Sheath/core type	0.117	122
PDO 70%	Sea/island type	0.182	99
PCL 30%	Sheath/core type	0.131	99

As shown in Table 13, the knot strength of the suture prepared by co-extruding the polymers to form the sea/island type is better than that of the suture prepared by co-extruding the polymers to form the sheath/core type. In addition, since the sea/island type suture is less stiff, its flexibility is greater.

Experimental Example 2

When a monofilament suture is prepared in a form such that the polymer having a low Young's modulus and a low melting point surrounds the polymer having a high Young's

modulus and a high melting point, the roundness of the suture is likely to be less during the drawing process. FIG. 4a is a photograph showing a cross section of a suture prepared by using polydioxanone having a high Young's modulus and a high melting point as the sea component, and polycaprolactone having a low Young's modulus and a low melting point as the island component. The suture was prepared under the conditions set forth in Example 1, and shows that the roundness of a cross section of the suture is good and its shape is stable. FIG. 4b is a photograph showing a cross section of a suture prepared by using polycaprolactone as the sea component and polydioxanone as the island component as in Comparative Example 1. The results show that the resulting shape is not suitable for use as a suture since there is significantly less roundness in cross section. When the suture has a cross section such as that seen in FIG. 4b, attachment of the needle to the suture is difficult. In practical use, a suture having the cross section shape as in FIG. 4b, which is nearly planar, is likely to cause tissue dragging.

Experimental Example 3

In order to show the beneficial effects of the present invention, the suture of the present invention was compared with sutures prepared by singly using polydioxanone and polycaprolactone, and a copolymer (Monocryl[®]) having improved flexibility. The results are set forth in Table 14 below.

Table 14

Comparison of the physical properties in accordance with the process for preparing a suture (EP 4 size)

Sample	Component	Stiffness (mgf/mm ²)	Knot slippage ratio (%)
PDO	Polydioxanone (single extrusion)	149	50
PCL	Polycaprolactone (single extrusion)	33	90
Example 1	Polydioxanone/Polycaprolactone (co-extrusion)	80	0
Monocryl [®]	Copolymer of glycolide and caprolactone (single extrusion)	105	60

As shown in Table 14, sutures made by co-extruding one polymer with polycaprolactone or copolymers thereof have significantly improved flexibility compared to those formed from the process of singly extruding polydioxanone. However, even though they have similar stiffness, the knot slippage ratio, as a barometer of knot security, varies

depending on the process used for preparing the suture. When polydioxanone and polycaprolactone were co-extruded, the knot did not slip at all, showing a knot slippage ratio of 0%. However, single extrusion of a homopolymer of polydioxanone, a homopolymer of polycaprolactone, and the copolymer of glycolide and caprolactone showed a knot slippage ratio of 50% or more..

When a knot is tied, normal force is added in a direction perpendicular to the length direction of the filament. If a polymer having a high Young's modulus is used as the first polymer, in accordance with the present invention, unevenness and/or cracking occurs at the site receiving the knot tying force as shown in FIGs. 5a and 5b, and the shape of the knot is easily deformed. Therefore, knot security is improved as the friction force of the surface increases.

FIGs. 6a and 6b are SEM photographs comparing the characteristics of the knot obtained by the present invention with that of a conventional suture. FIG. 6a represents the knot configuration of the sea/island monofilament suture obtained from Example 1. FIG. 6b represents the knot configuration of the sea/island monofilament suture using polylactide and polycaprolactone obtained from Experimental Example 5. FIG. 6c represents the knot configuration of the monofilament suture prepared by using polydioxanone only. As shown in FIGs. 6a and 6b, the shape deformation of the suture obtained by the present invention occurs upon tying a knot, so that when the suture is firmly tied, there is little space left in the knot. On the contrary, the knot in the suture of FIG. 6c has much space therein, and thus, the tied knot is easily loosened.

Experimental Example 4

This example illustrates the relationship of the content ratio of the first polymer and the second polymer with the shape of a cross section of the suture. Procedures were carried out under the same conditions described in Example 2 except that the number of the island component was 7. After carrying out the experiment, the shapes of cross sections of the sutures are shown in FIG. 7. FIG. 7a represents the cross section of a suture having the first polymer in an amount of 70% by volume. FIG. 7b represents the cross section of the suture having the first polymer in an amount of 50% by volume and FIG. 7c represents the cross section of a suture having the first polymer in an amount of 20% by volume.

As shown in FIG. 7c, when the amount of the first polymer is 20% by volume, the area that the second polymer occupies becomes greater. Therefore, since the thickness of the first polymer surrounding the second polymer is less, the drawability is likely to be less when

preparing this suture. Even when the suture is prepared, its shape is likely to be changed by the annealing process, and thus, the surface of the suture is apt to become rough. Therefore, in order to prepare a suture suitable for the purpose of the present invention, preferably, the amount of the first polymer is 20% or more by volume, and more preferably, 50% or more by volume.

Experimental Example 5

Poly lactide, having a Young's modulus of 2.7GPa and a melting point of 170~180°C, was used as the first polymer and polycaprolactone as the second polymer. A sea/island type monofilament suture was prepared by co-extruding the polymers in accordance with the parameters, terms and conditions as set forth in Table 15 below.

Table 15

Conditions of Processing the Sea/Island Type Co-extruded Suture

Suture Size		EP 4	
Polymer		Polycaprolactone	Poly lactide
Young's modulus (GPa)		0.7	2.7
Melting Point (°C)		55~65	170~180
Process Conditions		Extrusion Conditions	
Extruder		Ext. 1 (Island)	Ext. 2 (Sea)
Number of Island Component		19	-
Extruder screw, rpm		8.3	2.2
Manifold pressure (kgf/cm ²)		80	80
Temperature of Extruder (°C)	Zone 1	185	190
	Zone 2	188	192
	Zone 3	200	195
Temperature of Manifold (°C)		200	195
Temperature of Metering pump (°C)		200	195
Temperature of Nozzle Pack Die (°C)		200	
Capacity of Metering pump (cc/rev)		1.2	1.2
Revolution of Metering pump (rpm)		6.3	2.7
Temperature of Quenching bath (°C)		23	
Winding Speed of Undrawn yarn (m/min)		13.2	
		Drawing Conditions	
First Roller (m/min)		4	
Temperature of First Drawing Oven (°C)		120	
Second Roller (m/min)		17.7	
Temperature of Second Drawing Oven (°C)		120	
Third Roller (m/min)		18.6	
Total Drawing Ratio		4.7	

In order to compare physical properties, polydioxanone having a Young's modulus of 1.3 GPa as the first polymer and polycaprolactone as the second polymer were extruded under the same conditions as in Example 1, except that the winding speed and the drawing temperature were different.

Using the methods for measuring the physical properties explained above, diameter, knot strength, stiffness and knot slippage ratio of the prepared sutures were measured.

Table 16

Comparison of physical properties of sutures

Composition	Diameter (mm)	Knot strength (Kgf)	Stiffness (mgf/mm ²)	Knot slippage ratio (%)
PDO/PCL	0.481	4.22	75	0
PLA/PCL	0.409	1.12	98	0
PLA	0.458	-	245	-

As indicated in Table 16, both monofilament sutures prepared by co-extrusion in accordance with the present invention demonstrated excellent knot security with knot slippage ratios of 0%. In addition, the suture prepared by using polydioxanone as the first polymer was not stiff but very flexible, with excellent knot security. However, the suture prepared by using polylactide as the first polymer showed low flexibility, which is caused by the high Young's modulus of polylactide. Therefore, to prepare monofilament sutures having excellent knot security and flexibility, it is preferable to use polymers that have a Young's Modulus of 2.0GPa or less.

The above description will enable one skilled in the art to make a monofilament suture having improved knot security and flexibility. The sutures of the present invention are prepared by co-extruding a first absorbable polymer and a second absorbable polymer having a Young's modulus lower than the Young's modulus of the first polymer, wherein the first polymer surrounds the second polymer, said suture having improved knot security and flexibility. Although they are described to show the functionality of the monofilament suture of the present invention, these descriptions are not intended to be exhaustive. It will be immediately apparent to one skilled in the art that various modifications may be made without departing from the scope of the invention which is limited only by the following claims and their functional equivalents.